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Pressure Drop Calculation Models of Wellbore Fluid in Perforated Completion Horizontal Wells

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ABSTRACT

Perforated completion is a main method of horizontal well completion. Based on the mass conservation equation, the momentum conservation equation and the variable mass flow in the horizontal wellbore, pressure drop calculation models of the wellbore fluid are established in perforated completion of horizontal wells. The results of calculation and analysis show that the frictional pressure drop, acceleration pressure drop and mixing pressure drop have different effects on total pressure drop of the wellbore fluid, and the frictional pressure drop plays a major role while the acceleration pressure drop and mixing pressure drop have little influence. The liquid viscosity, production and horizontal wellbore length also have different effects on various kinds of pressure drop. When liquid viscosity is smaller and the length of the horizontal wellbore is shorter, the effects of the acceleration pressure drop and mixing pressure drop cannot be neglected. The theoretical basis and the calculation model of the variable mass flow pressure drop of horizontal wellbore are provided.

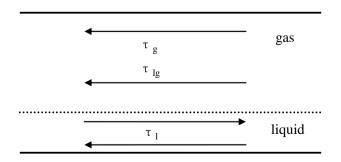
Keywords: Pressure drop of wellbore fluid, Variable Mass Flow, Stratified flow, Perforated completion, Horizontal well.

1. INTRODUCTION

In perforated completion of a horizontal well, due to variable mass flow of fluid in the horizontal wellbore, there is a drop in pressure along the horizontal wellbore, which will have an effect on fluid seepage and easily cause bottom water coning. Much research [1-23] has been done on pressure drop of horizontal wellbore. Scholars derived pressure drop model of horizontal wellbore, and obtained the variation law of pressure drop, as well as its impact on fluid flow. However this research has not considered the many forms of pressure drop which affect total pressure drop of horizontal wellbore systematically, without quantitatively analyzing the impact of all forms of pressure drop on total pressure drop, and considering the proportion of various forms of pressure drop to total pressure drop of a horizontal wellbore. Based on mass conservation equation and momentum conservation equation, this paper establishes a pressure drop model of perforated completion in a horizontal wellbore. It calculates and analyzes the impact of frictional pressure drop, acceleration pressure drop and mixing pressure drop on the total pressure drop in a horizontal wellbore. Furthermore, it analyzes the impact of viscosity, production, and length of a horizontal wellbore on the three kinds of pressure drop, as well as the impact boundary of acceleration pressure drop and mixing pressure drop on total pressure drop in a horizontal wellbore. It provides a theoretical basis and calculation model of pressure drop analysis of variable mass flow in perforated completion of a horizontal wellbore.

2. MODELING

It is assumed there is a gas/liquid two phase stratified flow in the horizontal wellbore as shown in Fig.1. The wellbore fluid is an isothermal flow, and there is no mass exchange in gas/liquid two phase. The pressure drop calculation model of horizontal wellbore is obtained from mass conservation equation and momentum conservation equation.



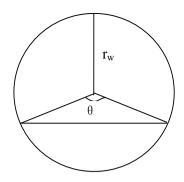


Figure 1. Gas-liquid two phase flow

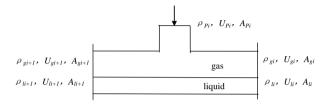


Figure 2. Balance of gas-liquid two phase flow

2.1 Mass conservation equation

$$\begin{cases}
\Delta(\rho_l \cdot A_l \cdot U_l) = m_l \Delta x \\
\Delta(\rho_g \cdot A_g \cdot U_g) = m_g \Delta x
\end{cases}$$
(1)

In the equation ρ_l is liquid density, kg/m³; ρ_g is gas density, kg/m³; A_l is liquid area, m²; A_g is gas area, m²; U_l is liquid velocity, m/s; U_g is gas velocity, m/s; m_l is liquid inflow per unit axis length, kg/(s·m); m_g is gas inflow per unit axis length, kg/(s·m); Δx is unit length, m.

Dividing both sides of the equation by Δx yields:

$$\begin{cases}
\frac{d\left(\rho_{l} \cdot A_{l} \cdot U_{l}\right)}{dx} = m_{l} \\
\frac{d\left(\rho_{g} \cdot A_{g} \cdot U_{g}\right)}{dx} = m_{g}
\end{cases} \tag{2}$$

Because:

$$A_l = \pi r_w^2 \cdot \alpha_l \tag{3}$$

$$A_{g} = \pi r_{w}^{2} \cdot \alpha_{g} \tag{4}$$

$$\alpha_l + \alpha_{_{\varrho}} = 1 \tag{5}$$

In the equation r_w is wellbore radius, m; α_l is liquid holdup of wellbore fluid, decimals; α_g is gas holdup of wellbore fluid, decimals.

Integrating equations (3) and (4) into equation (2) yields:

$$\begin{cases}
\frac{d\left(\rho_{l} \cdot U_{l} \cdot \alpha_{l}\right)}{dx} = \frac{m_{l}}{\pi r_{w}^{2}} \\
\frac{d\left(\rho_{g} \cdot U_{g} \cdot \alpha_{g}\right)}{dx} = \frac{m_{g}}{\pi r_{w}^{2}}
\end{cases} \tag{6}$$

In equation (6) [24]:

$$m_{l} = \frac{\ln\left(\frac{r_{ep}}{r_{p}}\right) - \sqrt{\ln\left(\frac{r_{ep}}{r_{p}}\right)^{2} - 4\frac{\rho_{l}\left(k_{rl}k\right)^{2}}{\mu_{l}^{2}}\beta_{l}\left(\frac{1}{r_{ep}} - \frac{1}{r_{p}}\right)\left(p_{ep} - p_{p}\right)}{\frac{k_{rl}k}{\pi\mu_{l}L_{p}}\beta_{l}\left(\frac{1}{r_{ep}} - \frac{1}{r_{p}}\right)}$$
(7)

$$m_{g} = \frac{\ln\left(\frac{r_{ep}}{r_{p}}\right) - \sqrt{\left[\ln\left(\frac{r_{ep}}{r_{p}}\right)\right]^{2} - 4\frac{\rho_{g}\left(k_{rg}k\right)^{2}}{\mu_{g}^{2}ZRT}\beta_{g}\left(\frac{1}{r_{ep}} - \frac{1}{r_{p}}\right)\left(p_{ep}^{2} - p_{p}^{2}\right)}}{\frac{k_{rg}k}{\pi\mu_{g}L_{p}}\beta_{g}\left(\frac{1}{r_{ep}} - \frac{1}{r_{p}}\right)}$$

In the equation, r_{ep} is equivalent perforation radius, m; r_p is inner perforation diameter, m; k_{rl} is relative permeability of liquid; k is formation permeability, μ m²; μ_l is liquid viscosity, mPa·s; β_l is velocity factor of liquid; P_{ep} is corresponding pressure of equivalent perforation radius, Pa; P_p is corresponding pressure of inner perforation diameter, Pa; k_{rg} is relative permeability of gas; μ_g is gas viscosity, mPa·s; Z is gas compression coefficient; R is coefficient of gas state equation; T is wellbore temperature, K; β_g is velocity factor of gas.

2.2 Momentum conservation equation

(1) Momentum conservation equation of liquid

$$\Delta \left(\rho_{l} \cdot A_{l} \cdot U_{l}^{2} \right) \cdot \Delta t = -\Delta P_{accl} \cdot A_{l} \cdot \Delta t - \Delta P_{mixl} \cdot A_{l} \cdot \Delta t - \tau_{l} S_{l} \Delta x \cdot \Delta t + \tau_{l} S_{l} \Delta x \cdot \Delta t$$

$$(9)$$

In the equation P_{accl} is acceleration pressure drop of liquid, Pa; P_{mixi} is mixing pressure drop of liquid, Pa; τ_l is shear stress of liquid and wall, Pa; τ_{lg} is shear stress of gas/liquid interface, Pa; S_l is liquid boundary length of flow cross section, m; S_{lg} is gas/liquid interface length, m; Δt is time of liquid flow through unit length, S.

(2) Momentum conservation equation of gas

$$\Delta \left(\rho_{g} \cdot A_{g} \cdot U_{g}^{2} \right) \cdot \Delta t = -\Delta P_{accg} \cdot A_{g} \cdot \Delta t - \Delta P_{mixg} \cdot A_{g} \cdot \Delta t - \tau_{g} S_{g} \Delta x \cdot \Delta t - \tau_{g} S_{lg} \Delta x \cdot \Delta t$$
(10)

In the equation P_{accg} is acceleration pressure drop of gas, Pa; P_{mixg} is mixing pressure drop of gas, Pa; τ_g is shear stress of gas and wall, Pa; S_g is gas boundary length of flow cross section, m.

(3) Momentum conservation equation of fluid

$$\begin{split} -\Delta P \cdot A \cdot \Delta t &= -\Delta P_{accl} \cdot A_l \cdot \Delta t - \Delta P_{mixl} \cdot A_l \cdot \Delta t - \tau_l S_l \Delta x \cdot \Delta t + \tau_{lg} S_{lg} \Delta x \cdot \Delta t \\ -\Delta P_{accg} \cdot A_g \cdot \Delta t - \Delta P_{mixg} \cdot A_g \cdot \Delta t - \tau_g S_g \Delta x \cdot \Delta t - \tau_{lg} S_{lg} \Delta x \cdot \Delta t \end{split} \tag{11}$$

In the equation P is total pressure drop of fluid, Pa. So:

$$\Delta \left(\rho_l \cdot A_l \cdot U_l^2 \right) \cdot \Delta t = -\Delta P \cdot A \cdot \Delta t + \Delta P_{accg} \cdot A_g \cdot \Delta t + \Delta P_{mixp} \cdot A_o \cdot \Delta t + \tau_o S_o \Delta x \cdot \Delta t + \tau_{lo} S_{lo} \Delta x \cdot \Delta t$$
(12)

$$\Delta \left(\rho_g \cdot A_g \cdot U_g^2 \right) \cdot \Delta t = -\Delta P \cdot A \cdot \Delta t + \Delta P_{accl} \cdot A_l \cdot \Delta t + \Delta P_{mixl} \cdot A_l \cdot \Delta t + \tau_l S_l \Delta x \cdot \Delta t - \tau_{lo} S_{lo} \Delta x \cdot \Delta t$$
(13)

Thereinto:

$$\Delta P_{accl} = \frac{3\rho_{l}U_{li}^{2} \cdot m_{lp} + 3U_{li} \cdot \frac{m_{lp}^{2}}{\pi r_{w}^{2} \cdot \alpha_{l}} + \frac{m_{lp}^{3}}{\rho_{l}^{2} \left(\pi r_{w}^{2} \cdot \alpha_{l}\right)^{2}} - m_{lp} \frac{1}{\rho_{l}} \left(\frac{m_{lp}}{\pi r_{p}^{2} \cdot \alpha_{l}}\right)^{2}}{2\rho_{l}\pi r_{w}^{2}U_{li} \cdot \alpha_{l} + m_{lp}}$$

 $\Delta P_{accg} = \frac{3\rho_g U_{gi}^2 \cdot m_{gp} + 3U_{gi} \cdot \frac{m_{gp}^2}{\pi r_w^2 \cdot \alpha_g} + \frac{m_{gp}^3}{\rho_g^2 (\pi r_w^2 \cdot \alpha_g)^2} - m_{gp} \frac{1}{\rho_g} \left(\frac{m_{gp}}{\pi r_p^2 \cdot \alpha_g}\right)^2}{2\rho_g \pi r_w^2 U_{gi} \cdot \alpha_g + m_{gp}}$ (15)

$$\Delta P_{mixl} = \frac{3 \cdot m_{lp}}{\pi r_{w}^{2}} \cdot \frac{U_{li}}{\alpha_{l}} + \frac{3m_{lp}^{2}}{2\rho_{l} (\pi r_{w}^{2})^{2}} \cdot \frac{1}{\alpha_{l}^{2}}$$

$$- \frac{3\rho_{l} U_{li}^{2} \cdot m_{lp} + 3U_{li} \cdot \frac{m_{lp}^{2}}{\pi r_{w}^{2} \cdot \alpha_{l}} + \frac{m_{lp}^{3}}{\rho_{l}^{2} (\pi r_{w}^{2} \cdot \alpha_{l})^{2}} - m_{lp} \frac{1}{\rho_{l}} \left(\frac{m_{lp}}{\pi r_{p}^{2} \cdot \alpha_{l}}\right)^{2}}{2\rho_{l} \pi r_{w}^{2} U_{li} \cdot \alpha_{l} + m_{lp}}$$

$$\Delta P_{mixg} = \frac{3 \cdot m_{gp}}{\pi r_{w}^{2}} \cdot \frac{U_{gi}}{\alpha_{g}} + \frac{3m_{gp}^{2}}{2(\pi r_{w}^{2})^{2}} \cdot \frac{1}{\rho_{g} \cdot \alpha_{g}^{2}}$$

$$- \frac{3\rho_{g} U_{gi}^{2} \cdot m_{gp} + 3U_{gi} \cdot \frac{m_{gp}^{2}}{\pi r_{w}^{2} \cdot \alpha_{g}} + \frac{m_{gp}^{3}}{\rho_{g}^{2} (\pi r_{w}^{2} \cdot \alpha_{g})^{2}} - m_{gp} \frac{1}{\rho_{g}} \left(\frac{m_{gp}}{\pi r_{p}^{2} \cdot \alpha_{g}}\right)^{2}}{2\rho_{g} \pi r_{w}^{2} U_{gi} \cdot \alpha_{g} + m_{gp}}$$
(17)

From Fig.1 yields:

$$S_l = r_w \cdot \theta \tag{18}$$

$$S_{g} = r_{w} \cdot (2\pi - \theta) \tag{19}$$

$$S_{\rm lg} = 2 \cdot r_{\rm w} \cdot \sin\left(\frac{\theta}{2}\right) \tag{20}$$

Dividing both sides of equation (12) by $\Delta t \cdot \Delta x$ yields:

$$\frac{d\left(\rho_{l}\cdot A_{l}\cdot U_{l}^{2}\right)}{dx} = -\frac{dP}{dx}\cdot A + \frac{dP_{accg}}{dx}\cdot A_{g} + \frac{dP_{mixg}}{dx}\cdot A_{g} + \tau_{g}S_{g} + \tau_{lg}S_{lg}$$
(21)

Integrating equations (3) and (4) into equation (21) yields momentum conservation equation of liquid:

$$\frac{d\left(\rho_{l}\cdot U_{l}^{2}\cdot\alpha_{l}\right)}{dx} = -\frac{dP}{dx} + \frac{dP_{accg}}{dx}\cdot\alpha_{g} + \frac{dP_{mixg}}{dx}\cdot\alpha_{g} + \frac{\tau_{g}}{\pi r_{w}^{2}}S_{g} + \frac{\tau_{lg}}{\pi r_{w}^{2}}S_{lg}$$
(22)

The momentum conservation equation of gas is similarly obtained:

$$\frac{d\left(\rho_{g} \cdot U_{g}^{2} \cdot \alpha_{g}\right)}{dx} = -\frac{dP}{dx} + \frac{dP_{accl}}{dx} \cdot \alpha_{l} + \frac{dP_{mixl}}{dx} \cdot \alpha_{l} + \frac{\tau_{l}}{\pi r_{w}^{2}} S_{l} - \frac{\tau_{lg}}{\pi r_{w}^{2}} S_{lg}$$
(23)

2.3 Calculation model of horizontal wellbore pressure drop

Combining mass conservation Eq(6) and momentum conservation Eq (22), (23) yields:

$$\begin{cases}
\frac{d\left(\rho_{l} \cdot U_{l} \cdot \alpha_{l}\right)}{dx} = \frac{m_{l}}{\pi r_{w}^{2}} \\
\frac{d\left(\rho_{g} \cdot U_{g} \cdot \alpha_{g}\right)}{dx} = \frac{m_{g}}{\pi r_{w}^{2}} \\
\frac{d\left(\rho_{l} \cdot U_{l}^{2} \cdot \alpha_{l}\right)}{dx} = -\frac{dP}{dx} + \frac{dP_{accg}}{dx} \cdot \alpha_{g} + \frac{dP_{mixg}}{dx} \cdot \alpha_{g} + \frac{\tau_{g}}{\pi r_{w}^{2}} S_{g} + \frac{\tau_{lg}}{\pi r_{w}^{2}} S_{lg} \\
\frac{d\left(\rho_{g} \cdot U_{g}^{2} \cdot \alpha_{g}\right)}{dx} = -\frac{dP}{dx} + \frac{dP_{accl}}{dx} \cdot \alpha_{l} + \frac{dP_{mixl}}{dx} \cdot \alpha_{l} + \frac{\tau_{l}}{\pi r_{w}^{2}} S_{l} - \frac{\tau_{lg}}{\pi r_{w}^{2}} S_{lg}
\end{cases} (24)$$

Eq(24) can be resolved by the fourth order Runge-Kutta

3. RESULT ANALYSIS

(16)

Basic data of wellbore pressure drop analysis of perforated completion model in horizontal well is shown in Tab. 1.

Table 1. Based data of pressure drop analysis model in horizontal well

Equivalent drainage radius(m)374Reservoir thickness (m)20Horizontal wellbore length(m)419Effective wellbore diameter (m)0.1594Effective perforation depth(m)0.55Effective perforation radius (m)0.006Permeability(μm²)0.06Toe end pressure of horizontal wellbore (MPa)20Initial perforation density (hole/m)20Total production(m³/d)7560Liquid density(kg/m³)900Liquid viscosity(mPa s)50Coefficient of gas state equation (J/kg/K)200Gas viscosity(mPa s)0.02Relative liquid permeability0.2Wellbore temperature(K)380Non-Darcy flow coefficient2.33Relative gas permeability0.8Friction coefficient0.316Index of friction coefficient0.19Initial liquid holdup0.04Gas compressibility1				
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Permeability(μm²) 0.06 (MPa) horizontal wellbore (MPa) 20 Initial perforation density (hole/m) 20 Total production(m³/d) 7560 Liquid density(kg/m³) 900 Liquid viscosity(mPa s) 50 Coefficient of gas state equation (J/kg/K) 200 Gas viscosity(mPa s) 0.02 Relative liquid permeability 0.2 Wellbore temperature(K) 380 Non-Darcy flow coefficient 2.33 Relative gas permeability 0.8 Friction coefficient 0.316 Index of friction coefficient 0.19		0.55		0.006
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density(kg/m³) Coefficient of gas state equation (J/kg/K) Relative liquid permeability Non-Darcy flow coefficient Priction coefficient 0.316 Liquid viscosity(mPa s) Gas viscosity(mPa s) 0.02 Wellbore temperature(K) Relative gas permeability 0.8 Index of friction coefficient 0.19		20	Total production(m ³ /d)	7560
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permeability 0.2 temperature(K) 380 Non-Darcy flow coefficient 2.33 Relative gas permeability 0.8 Friction coefficient 0.316 Index of friction coefficient 0.19	state equation	200	Gas viscosity(mPa s)	0.02
coefficient 2.33 permeability 0.8 Friction coefficient 0.316 Index of friction coefficient 0.19		0.2		380
Friction coefficient 0.316 coefficient 0.19	•	2.33	~	0.8
Initial liquid holdup 0.04 Gas compressibility 1	Friction coefficient	0.316		0.19
	Initial liquid holdup	0.04	Gas compressibility	1

3.1 Component analysis of total pressure drop in horizontal wellbore

Pressure drop of fluid in horizontal wellbore consists of three parts: (1) frictional pressure drop caused by gas/liquid interaction as well as friction of gas/liquid and wellbore wall; (2) inflowing fluid through perforation mixes with fluid in horizontal wellbore, and fluid redistribution causes mixed pressure drop; (3) radial flow and liquid holdup change causes flow rate change of gas and liquid, which contributes to acceleration pressure drop. Calculation result is shown in Fig. 3.

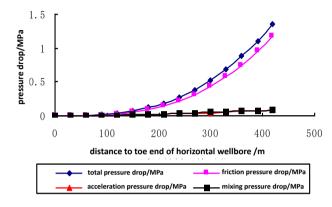


Figure 3. Various types of pressure drop curve in horizontal wellbore

Fig. 3 shows that when fluid flows through toe end to heel end of the horizontal wellbore, the total pressure drop of the horizontal wellbore is 1.36MPa. Friction pressure drop accounts for more than 85%, while the percentage of acceleration pressure drop and mixed pressure drop is relatively small.

3.2 Impact of viscosity on horizontal wellbore pressure drop

While other conditions remain unchanged, with liquid viscosity of 50mPa·s, 100mPa·s, 500mPa·s, 1000mPa·s, 5000mPa·s, 1000mPa·s, 5000mPa·s and 10000mPa·s, the total pressure drop curve is shown in Fig. 4, friction pressure drop curve is shown in Fig. 5, acceleration pressure drop curve is shown in Fig. 6, and mixed pressure drop curve of horizontal wellbore is shown in Fig. 7.

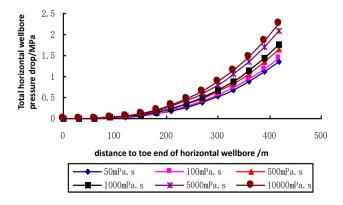


Figure 4. General pressure drop curve in horizontal wellbore

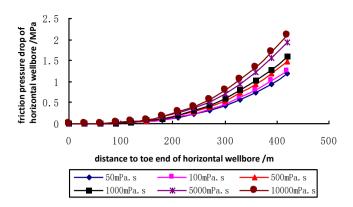


Figure 5. Frictional pressure drop curve in horizontal wellbore

Fig. 4 and Fig. 5 show that when liquid viscosity increases, total pressure drop and friction pressure drop increase gradually. The impact of liquid viscosity on total pressure drop and friction pressure drop in horizontal wellbore is obvious.

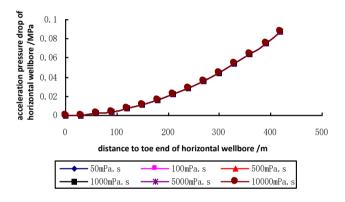


Figure 6. Acceleration pressure drop curve in horizontal wellbore

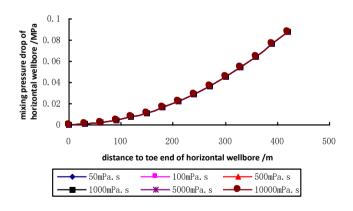


Figure 7. Mixing pressure drop curve in horizontal wellbore

Fig. 6 and Fig. 7 show that liquid viscosity has less influence on accelerating pressure drop and mixing pressure drop in horizontal wellbore.

3.3 Impact of production on horizontal wellbore pressure drop

While other conditions remain unchanged, with production of 100m³/d, 500m³/d, 1000m³/d, 5000m³/d, 8000m³/d and 10000m³/d, the total pressure drop curve is shown in Fig. 8, friction pressure drop curve is shown in Fig. 9, acceleration pressure drop curve is shown in Fig. 10, and mixing pressure drop curve of horizontal wellbore is shown in Fig. 11.

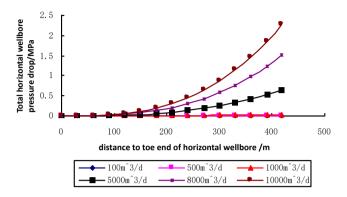


Figure 8. Total pressure drop curve in horizontal wellbore

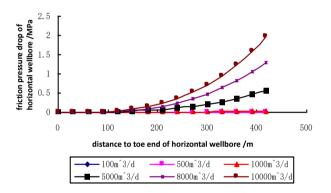


Figure 9. Friction pressure drop curve in horizontal wellbore

Fig. 8 and Fig. 9 show that production has a large effect on total pressure drop and friction pressure drop in the horizontal wellbore. When production increases, total pressure drop and friction pressure drop in the horizontal wellbore increase gradually.

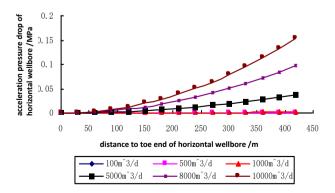


Figure 10. Acceleration pressure drop curve in horizontal wellbore

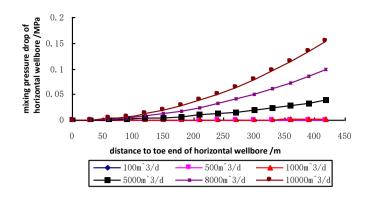


Figure 11. Mixing pressure drop curve in horizontal wellbore

Fig. 10 and Fig. 11 show that production also has a large effect on acceleration pressure drop and mixing pressure drop in the horizontal wellbore. When production increases, acceleration pressure drop and mixing pressure drop in the horizontal wellbore increase gradually.

3.4 Impact of horizontal section length on horizontal wellbore pressure drop

While other conditions remain unchanged, with horizontal section length of 200m, 500m, 800m, 1000m, 1500m and 2000m, the total pressure drop curve is shown in Fig. 12, friction pressure drop curve is shown in Fig. 13, acceleration pressure drop curve is shown in Fig. 14, and mixing pressure drop curve of horizontal wellbore is shown in Fig. 15.

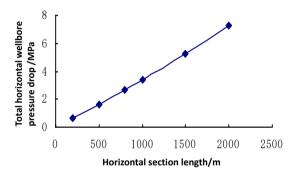


Figure 12. General pressure drop curve in horizontal wellbore

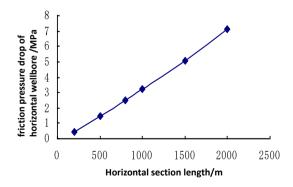


Figure 13. Friction pressure drop curve in horizontal wellbore

Fig. 12 and Fig. 13 show that the horizontal section length has a large effect on total pressure drop and friction pressure drop in the horizontal wellbore. When the horizontal section length increases, total pressure drop and friction pressure drop in the horizontal wellbore increase gradually.

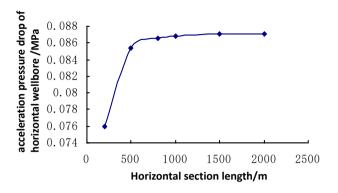


Figure 14. Acceleration pressure drop curve in horizontal wellbore

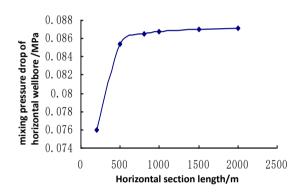


Figure 15. Mixing pressure drop curve in horizontal wellbore

Fig. 14 and Fig. 15 show that the horizontal section length has less effect on acceleration pressure drop and mixing pressure drop in horizontal wellbore. When the horizontal section length increases, acceleration pressure drop and mixing pressure drop in the horizontal wellbore increase gradually, but increasing amplitude decreases.

3.5 Impact boundary of acceleration pressure drop on total pressure drop in horizontal wellbore

When acceleration pressure drop is less than 5% of the total wellbore pressure drop, the impact of acceleration pressure drop on the total horizontal wellbore pressure drop is negligible; but when acceleration pressure drop is more than 5% of the total wellbore pressure drop, the impact of acceleration pressure drop on the total horizontal wellbore pressure drop must be considered. From the above analysis, the main factors that affect total horizontal wellbore pressure drop are liquid viscosity, production and horizontal section length. Friction pressure drop is mainly influenced by liquid viscosity, production and horizontal section length. Acceleration pressure drop and mixing pressure drop are mainly influenced by the horizontal section length. With a horizontal well production of 7560m³/d, the relation curve indicating the impact boundary of acceleration pressure drop on total horizontal wellbore pressure drop is shown in Fig 16, where μ is liquid viscosity, mPa·s. To liquid viscosity and horizontal section length, when eligible points are at the bottom-left of the curve, the impact of accelerating pressure drop on the total horizontal wellbore pressure drop is negligible. When they are at the top-right of the curve, the impact of acceleration pressure drop on total horizontal wellbore pressure drop must be considered.

Similarly the impact boundary of mixing pressure drop on total horizontal wellbore pressure drop is shown in Fig. 17.

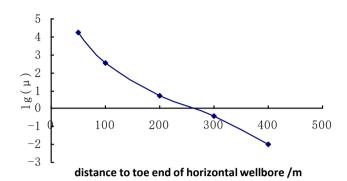


Figure 16. Boundary curve of accelerating pressure drop impact on general pressure drop

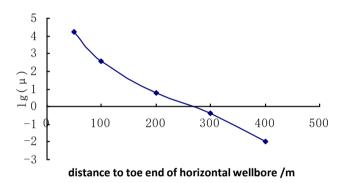


Figure 17. Boundary curve of mixing pressure drop impact on total pressure drop

4. CONCLUSIONS

- (1) Considering variable mass flow of fluid in the horizontal wellbore, based on mass conservation equation and momentum conservation equation, the pressure drop model of perforated completion in horizontal wellbore is established. In order to analyze, the total horizontal wellbore pressure drop is divided into friction pressure drop, acceleration pressure drop and mixing pressure drop. This provides a theoretical basis and calculation model for pressure drop analysis of variable mass flow in horizontal wellbore.
- (2) Normally, friction pressure drop plays a leading role in total horizontal wellbore pressure drop. Accelerating pressure drop and mixing pressure drop has less effect on the total horizontal wellbore pressure drop.
- (3) Liquid viscosity mainly affects the total horizontal wellbore pressure drop by friction pressure drop. When liquid viscosity is of a higher degree, friction pressure drop and total pressure drop of the horizontal wellbore is larger. Horizontal well production has an obvious effect on total horizontal wellbore pressure drop, friction

pressure drop, acceleration pressure drop, and mixing pressure drop. With an increase in horizontal well production, many types of pressure drop in the horizontal wellbore increases. Horizontal section length mainly affects the total horizontal wellbore pressure drop by effect of horizontal wellbore friction pressure drop, and it has less effect on accelerating pressure drop and mixing pressure drop.

(4) The impact boundary of acceleration pressure drop and mixing pressure drop on total horizontal wellbore pressure drop has been studied, and the boundary curve plate has been obtained.

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