

Numerical simulation of the compressible flow in convergent-divergent nozzle

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ABSTRACT

This work concerns the numerical simulation of a non-reactive turbulent flow of a compressible fluid (air) in a convergent divergent nozzle. The numerical study of this turbulent nozzle flow has been carried out by solving the Reynolds averaged Navier-Stokes equations. We have also used the two transport equations of type (k, ω) SST (Shear-Stress-Transport) of Menter to model the turbulence. The finite volume method is used to solve the system of equations. McCormack scheme has been used. The present results are compared with experimental results of the literature. In order to study the pressure influence on the flow characteristics such as speed pressure and temperature, etc. and particularly delamination phenomenon. These results are represented by field's contours and variable flow profiles of the axis of the nozzle and near the wall.

Keywords: CFD, Converging-diverging Nozzle, Compressible Flow 2D, Finite Volume, Shock Wave, Supersonic, Turbulence Flow.

1. INTRODUCTION

The problems of fluid dynamics are often difficult to solve because the system of equations governing the phenomenon which is strongly nonlinear system. It is difficult to find exact solutions. However, CFD (Computational Fluid Dynamics) technology especially the calculation applied to fluid dynamics change was successful; these successes are due to the close interaction between theory, numerical simulation and experimentation in fluid dynamics. On the one hand, experience is essential to test the hypotheses and the results that emerge from the theory [1]; on the other hand, the theory is needed to explain the results. Numerical simulation is independent of experience, it is necessary for the validation of experimental results.

The results are presented for nozzle flow subsonic - supersonic. Various numerical tests presented in this study relate to the influence of the variation of the geometry of the nozzle such that the angle of divergence as well as the effect of the variation of the input of the characteristic quantities of the pressure flows.

2. TURBULENCE MODELLING

As part of the fluid mechanics treatment of turbulence, the use of Reynolds decomposition applied to the solutions of the Navies-Stokes equation simplifies the problem by eliminating the fluctuations of periods and short amplitudes.

The numerical results obtained detected the different phenomena observed experimentally.

Using the finite volume method Mac Cormack is used for solving mathematical model equations.

The turbulence model used is that of the two additional transport equations $k-\omega$ SST Menter used to describe turbulence as summarized below:

$$\frac{D\rho k}{Dt} = \tau_{ij} \frac{\partial U_i}{\partial x_j} - \beta^* \rho \omega k + \frac{\partial}{\partial x_k} \left[\frac{(\mu + \sigma_k \mu_t) \partial k}{\partial x_k} \right] \quad (1)$$

$$\begin{aligned} \frac{D\rho\omega}{Dt} = & \frac{\gamma}{v_t} \tau_{ij} \frac{\partial U_i}{\partial x_j} - \rho \beta \omega^2 + \frac{\partial}{\partial x_k} \left[\frac{(\mu + \sigma_k \mu_t) \partial k}{\partial x_k} \right] \\ & + \frac{2\rho(1-F_1)\sigma_\omega^2}{\dot{u}} \frac{\partial k}{\partial x_j} \frac{\partial \omega}{\partial x_j} \end{aligned} \quad (2)$$

The left hand side of the Eqs. (1) and (2) is the Lagrangian derivative $\frac{D}{Dt} = \frac{\partial}{\partial t} + U_i \frac{\partial}{\partial x_i}$ and the turbulent stress tensor σ_{ij} is given by:

$$\tau_{ij} = \mu_t \left[\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} - \frac{2}{3} \frac{\partial U_k}{\partial x_k} \delta_{ij} \right] - \frac{2}{3} \rho k \delta_{ij} \quad (3)$$

The function F_1 is designed to blend the model coefficients of the original $k-\omega$ model in boundary layer zones with the transformed $k-\omega$ model in free shear layer and free stream zones. This function is expressed in term of local variables as:

$$F_1 = \tanh\left(\min\left(\max\left(\left[\frac{2\sqrt{k}}{0.09\omega y'} \frac{500v}{y^2\omega}, \frac{4\rho\sigma_{\omega 2}k}{CDk\omega y^2}\right]\right)\right)\right) \quad (4)$$

where $CDk\omega$ is a cross diffusion term added in Eq. (4)
According to Bradshaw's [8] assumption the eddy viscosity is defined in the following way:

$$\mu_t = \frac{a_1 k}{\max(a_1 \omega, |\Omega|) F_2} \quad (5)$$

where F_2 is a function that is one for the boundary-layer flows and zero for the free shear layers

With:

$$|\Omega| = \sqrt{2\Omega_{ij}\Omega_{ij}}$$

$$F_2 = \tanh(ar g_2)$$

$$ar g_2 = \max\left[\frac{2\sqrt{k}}{0.09y\omega'} \frac{500v}{y^2\omega}\right]$$

2.1 Reliability condition in turbulence models

The two-equation turbulence models are based on the Boussinesq assumptions where the Reynolds stresses is expressed as a linear function of the mean strain tensor:

$$-\rho u_i u_j = \frac{2C_\mu \rho k^2}{\varepsilon} \left(S_{ij} - \frac{1}{3} S_{ii} \right) - \frac{2}{3} \rho k \delta_{ij} \quad (6)$$

where C_μ as shown by V. P. Lebedev and al. [3] these equations can give negative values of the normal stress if S_{ij} is too large. Bradshaw [8] has noticed that in two-dimensional boundary layers submitted to a strong pressure gradient the shear stress was approximately proportional to the turbulent kinetic energy with:

$$-\bar{uv} \approx \sqrt{C_\mu k} \quad (7)$$

These two remarks led to introduction of weakly non-linear turbulence models in which the C_μ factor is allowed to vary according to:

$$C_\mu = \min\left(0.09, \frac{1}{A_0 + A_S (S^2 + A_\Omega \Omega^2)^{1/2}}\right) \quad (8)$$

With:

$$\begin{cases} S = \frac{1}{\omega \beta^*} \sqrt{2 S_{ij} S_{ij} - \frac{2}{3} S_{kk}^2}, \\ S_{ij} = \frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right), \\ \Omega = \frac{1}{\omega \beta^*} \sqrt{2 \Omega_{ij} \Omega_{ij}}, \\ \Omega_{ij} = \frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) \end{cases} \quad (9)$$

And $A_0 = 0, A_s = 2, A_\Omega = 0$ in this case the Bradshaw [8] coefficient (0.31) is substituted by $C_\mu^{1/2}$ in the formulation of the eddy viscosity.

3. NUMERICAL METHOD

The Navier-Stokes energy turbulence model equations are solved on a computational domain of variables ζ and η (transformed coordinates of the physical domain), by the use of finite volumes predictor-corrector. The new system of equations is solved by using MacCormack's explicit-implicit scheme [4]. This algorithm is second-order accurate in space and time. The basic discretization for the convective fluxes is modified to account for the physical properties of information propagation, as done initially by R. F. Cuffel, L. H. Back, and P. F. Massier [5]. The flux splitting is made second order accurate, but in shock regions where it is lowered to first order. The viscous terms are centered and the axisymmetric source terms are integrated at the Centre of each control volume in both the ζ and η directional sweeps. To reach a steady-state solution with a minimum number of iterations, the explicit discretization is complemented with an implicit numerical [7] approximation which is free from stability conditions.

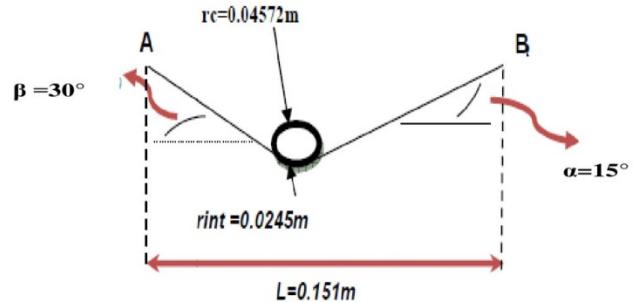


Figure 1. Nozzle geometry

4. VALIDATION

The present model is compared with the results due to Back and al. [4]. As shown in Figures 2a and 2b, static to stagnation pressure ratio is in good agreement between the two works.

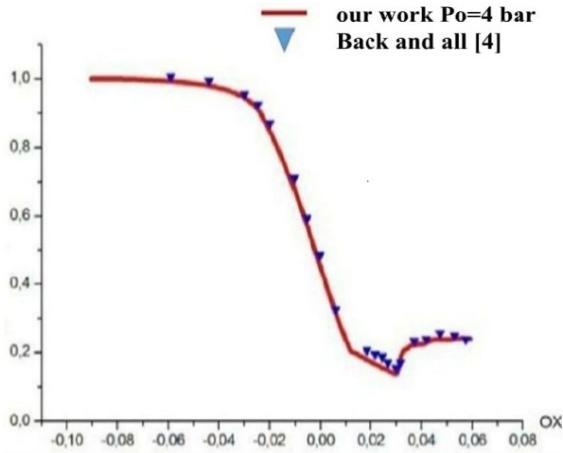


Figure 2a. Ratio of the pressure comparison between our works And that of Back and al. [4]

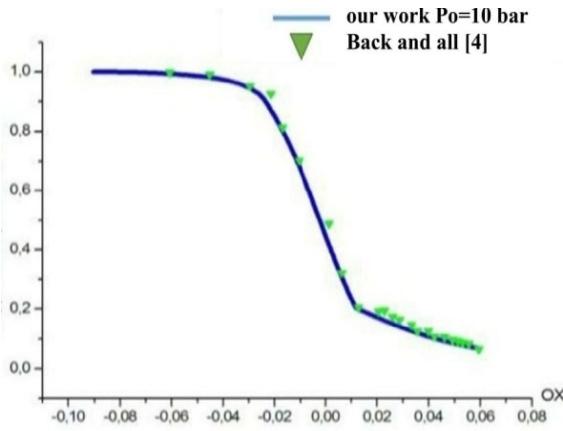


Figure 2b. Ratio of the pressure comparison between our works and that of Back and al. [4]

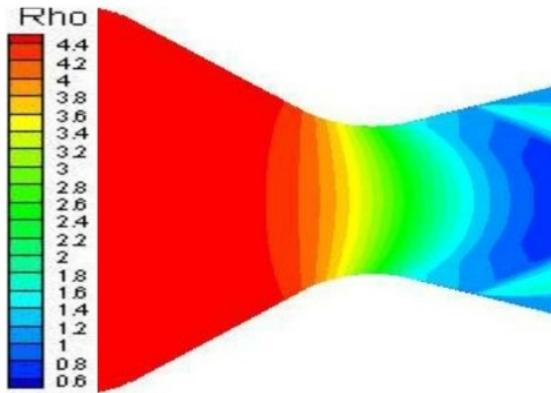


Figure 3. Contours of density (kg / m^3) ($\text{Po}=4 \text{ bar}$)

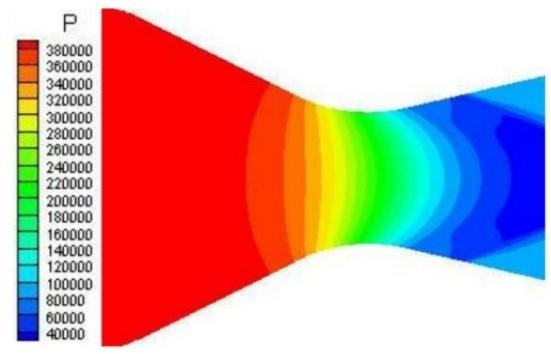


Figure 4a. Contours of Static Pressure (pa)

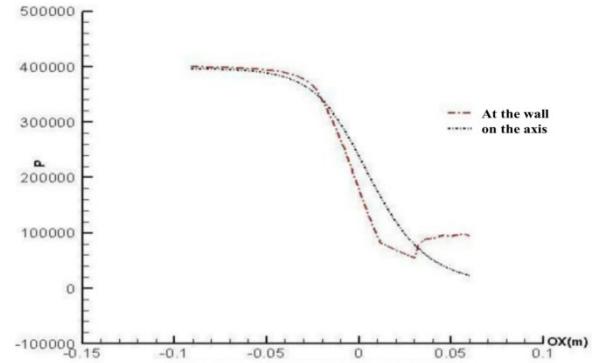


Figure 4b. Evolution of static pressure center and cell wall ($\text{Po}=4 \text{ bar}$)

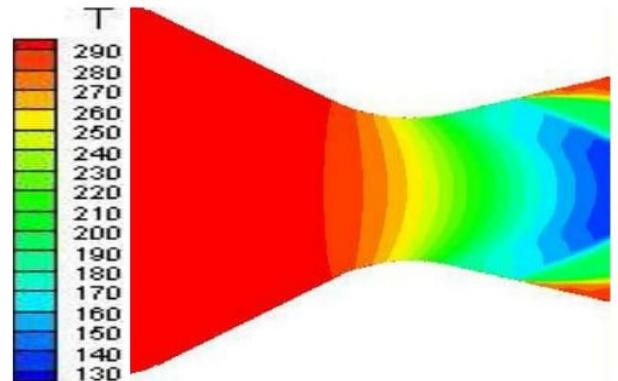


Figure 5a. Contours of temperature (K)

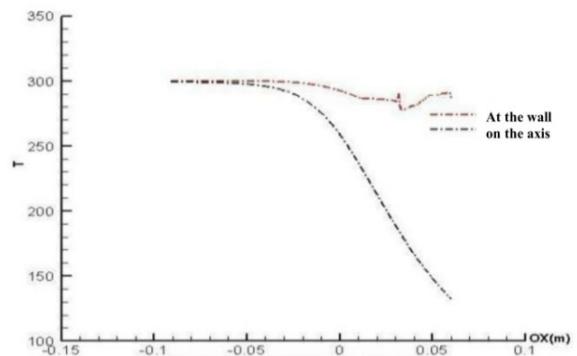


Figure 5b. Evolution of temperature center and cell wall (K) ($\text{Po}=4 \text{ bar}$)

Figure 3 shows the density profile (color change) that takes two different paths; the first surface from the entrance of the nozzle to its neck, the density in this part is almost constant at its maximum value. The second surface that begins just after the neck of the nozzle, the density undergoes a small increase and then continues to decrease until the exit of the nozzle.

The pressure drop inside the nozzle is shown schematically in Figures 4a and 4b. qualitatively this profile follows almost the same form of density profile.

The temperature distribution and its evolution are shown respectively in Figs. 5a and 5b, the temperature in the middle of the nozzle is subject to a homogeneous and continuous descent until the exit.

The wall is slightly reduced with a small increase in different inputs before exiting the nozzle (shock wave), on the other hand the proportion of fixed wall distribution along the nozzle due to the friction between flow and walls.

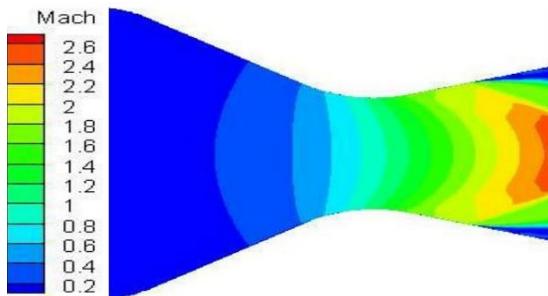


Figure 6a. Contours of Mach number

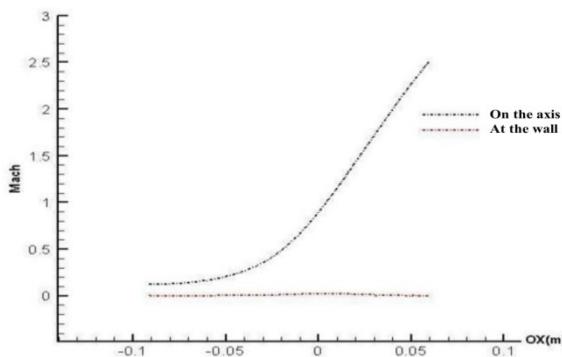


Figure 6b. Evolution of Mach number center and cell wall ($P_0=4$ bar)

The evolution of the Mach number on the centre and the wall of the nozzle shown in Figures 6a and 6b respectively, we observe that the regime at the inlet of the nozzle remains almost constant or invariable up to axis of the nozzle. We can say that the regime is subsonic ($Ma < 1$). We can neglect the air compressibility for Mach numbers less than 0.3, because the value of the Mach number is strictly less than unity, then there is a sharp increase in the vicinity of the neck of the nozzle exactly between the first point of tangency at the convergence and the first point of tangency in the divergent. In this zone the regime becomes transonic ($0.94 < Ma < 1.2$), because there is a small decrease on the centre of the nozzle. At the entrance of the diverging zone, the value of Mach number inside the nozzle continues to increase until the exit of the nozzle in this zone, the regime is hypersonic ($Ma > 5$). The same observations for the evolution of the Mach number except in parietal disturbance in the vicinity of the neck due to friction between the fluid and the wall. The convergent-divergent profile of the nozzle accelerates the gas from subsonic speed to supersonic speed that causes the displacement.

5. CONCLUSION

This computational result examined the effects of several parameters on the dynamic and thermal characteristics of flow

through a cooled convergent-divergent nozzle. The computational results indicated the following:

For an initial pressure, P_0 , inferior to the critical pressure, P_c , the delamination position is affected by this pressure difference and moves the nozzle throat. On the other hand, if the initial pressure is greater than the critical pressure, the release moves the lip of the nozzle until its disappearance which is desirable. Therefore, the delamination, which is an undesirable, phenomenon, appears in some flows, particularly when the initial pressure is below to the critical pressure. This could be causes the degradation of nozzle aerodynamic performances and efficiency and also causes noise and structure vibrations. So, in order to avoid these disadvantages, it is important to increase the initial pressure and make an optimal choice of the nozzle outlet angle.

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NOMENCLATURE

k	turbulent kinetic energy
ω	specific turbulent dissipation rate
μ	dynamic viscosity
ρ	turbulent viscosity
Ω	scalar measure of the vortices tensor
Ω_{ij}	vortices tensor
γ	specific heat ratio
a_1	brdshow constant

r	radius, radial coordinate, recovery factor	e	free stream condition
x	axial coordinate	F_1, F_2	auxiliary functions in turbulence model
T	Temperature	t	Time
Ma	Mach number	Subscripts	
P	Pressure	0	nozzle entrance condition
Pr_t	turbulent Prandtl number	th	throat position
U_i	mean velocities	sep	separation position
u_i	fluctuating velocities	w	parameters on the wall surface
h	heat transfer coefficient	aw	adiabatic wall
Pr	Prandtl number		